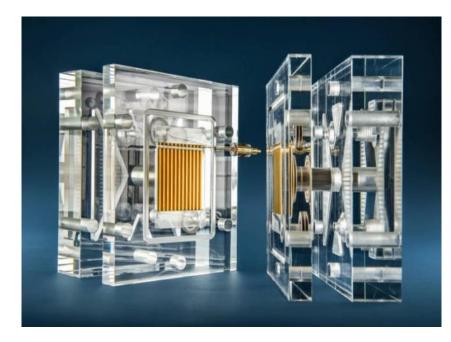
Electrochemical impedance spectroscopy (EIS) and half-cell potential measurements as tools for degradation analysis and AST development within PEM water electrolysis test cells



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Outline

- Motivation
- Development of AST protocols
- Test equipment at Fraunhofer ISE
- In-situ characterization method development
- Conclusion



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Motivation Why do we need ASTs?

PEM electrolysis cells are electrochemically stable, degradation occurs slowly

 \rightarrow Investigation of the degradation on materials is cost intensive

- Cheaper and more efficient stacks are required in the future
- New materials are needed, where degradation behaviour is unknown
 - \rightarrow Fast screening of these materials and profiles necessary



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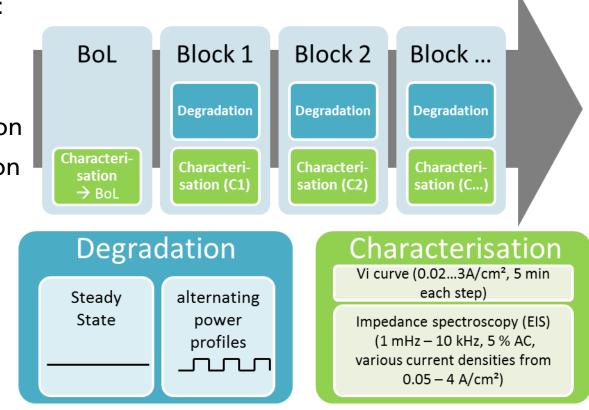


Development of AST protocols Our Approach for characterization

Operating conditions:

- Current density
- Temperature
- H₂O contamination
- Dynamic operation

Pressure



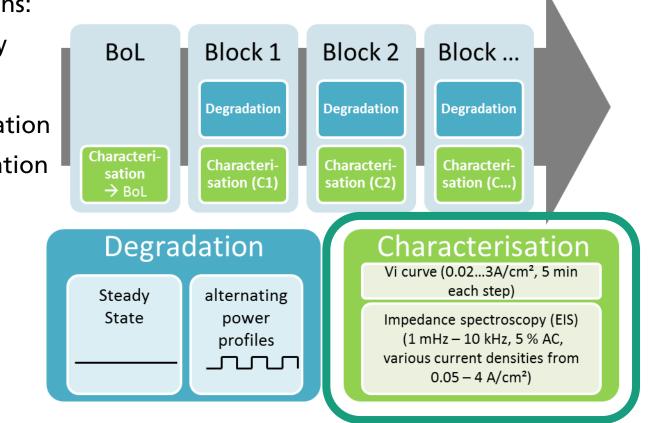


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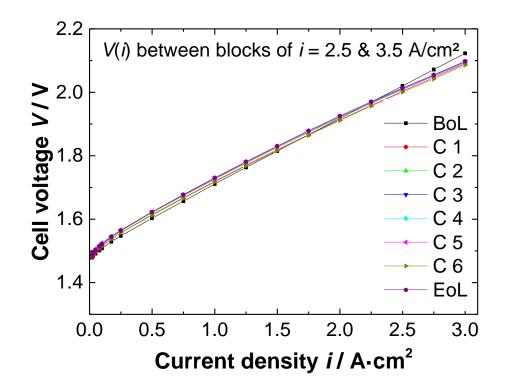




Development of AST protocols

Why do we need in-situ charactization methods?

- Vi(t) changes are rather small (within ≈ 340 h)
- Information content in Vi is limited

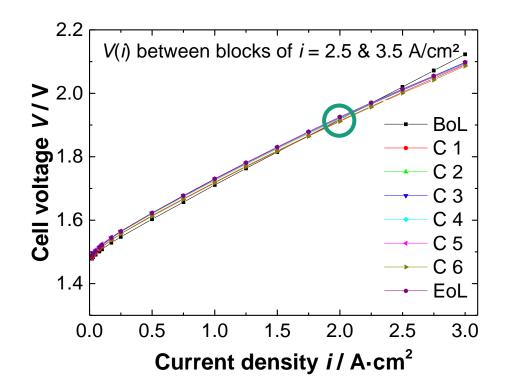




Development of AST protocols

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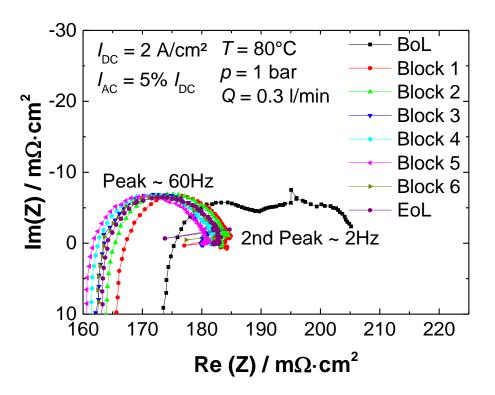


Development of AST protocols

Why do we need in-situ charactization methods?

- Vi(t) changes are rather small (within ≈ 340 h)
- Information content in Vi is limited
- Information content in EIS more comprehensive

→ Further characterization method development is very important



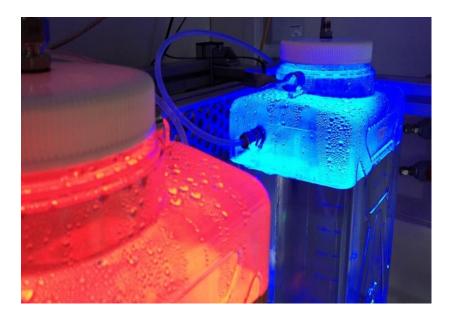


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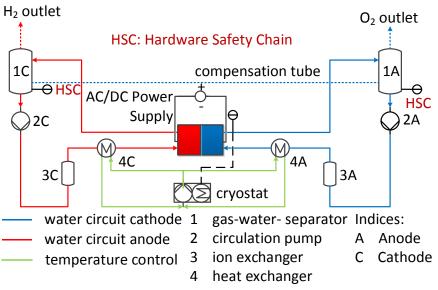


Test equipment at Fraunhofer ISE Non-automated, unpressurized test bench



- Impedance spectroscopy
 up to i_{DC} = 4 A/cm² (25 cm²)
 - *f* = 0.1 Hz 10 kHz

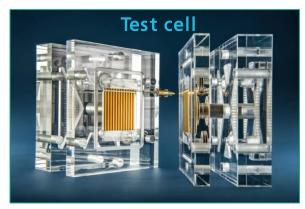
- Operation temperature up to 80°C
- Ivium 4 channel potentiostat
 + 100 A Ivium booster



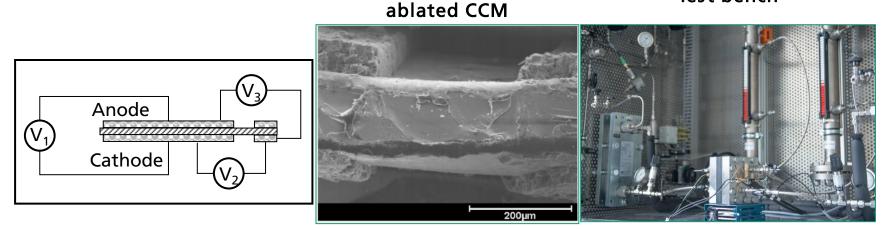


Test equipment at Fraunhofer ISE Cell setup with in-situ overpotential measurement

- Investigation of anodic and cathodic overpotentials
- Reference electrode made by laser ablation
- Pressurized measurements up to 50 bar
- Cell area of 25 cm² (including reference electrode)
 Cross-section of a laser



Test bench





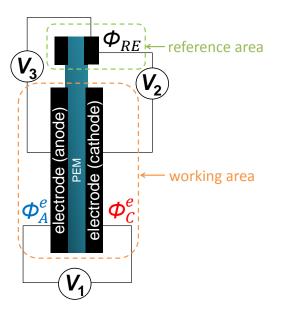
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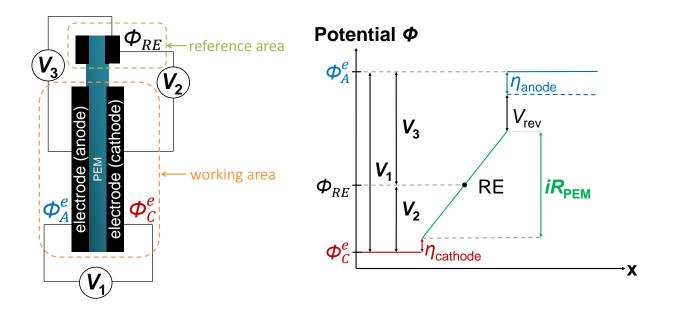






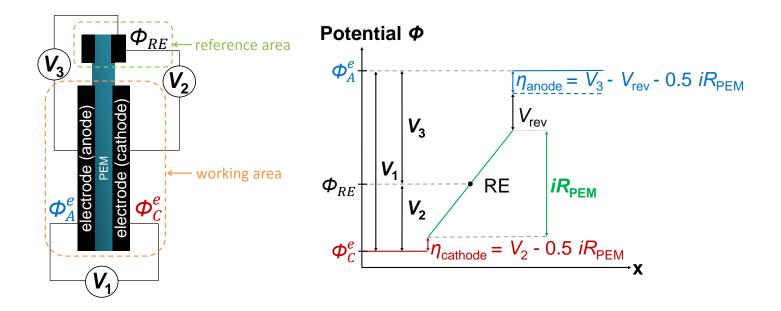
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Assumption that potential in the middle of the membrane is measured



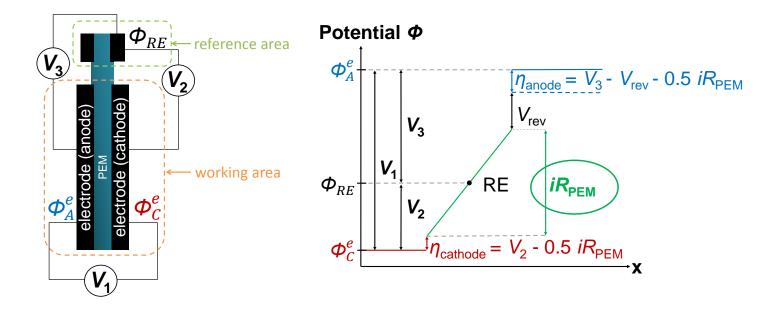


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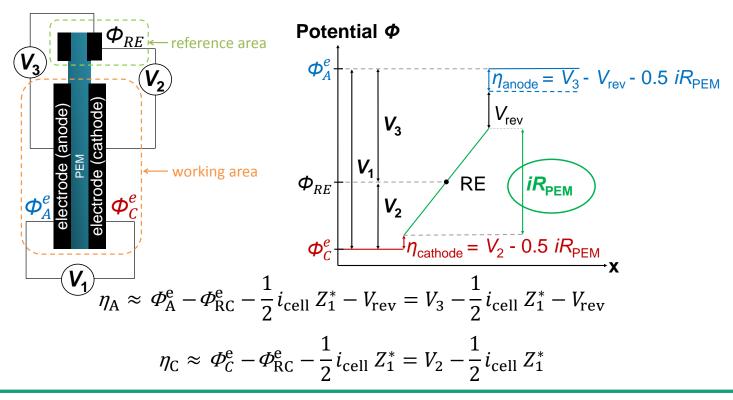
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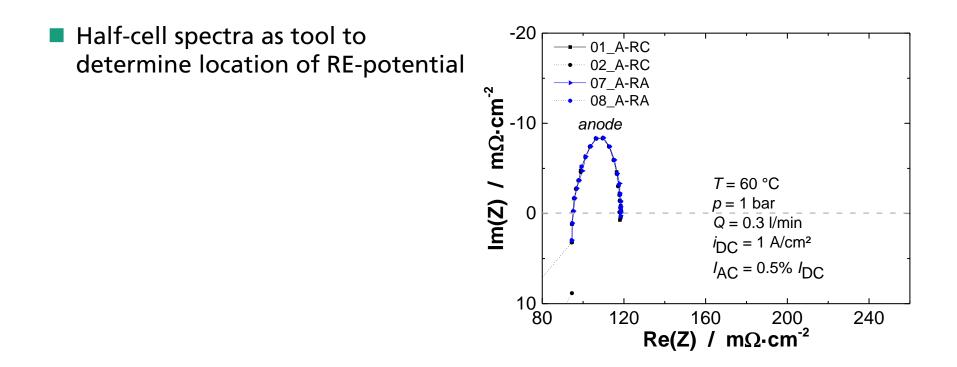


Assumption that potential in the middle of the membrane is measured

High frequency resistance (HFR) is measured by impedance spectroscopy

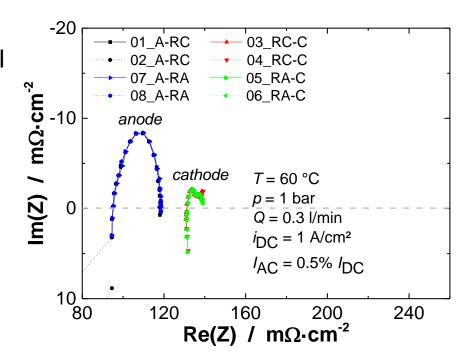






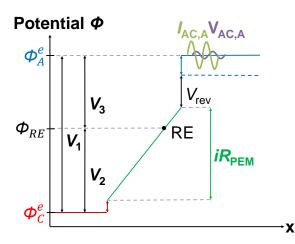


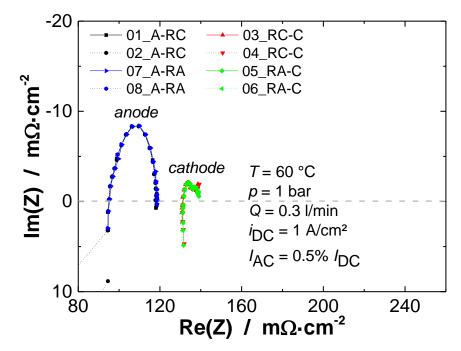
- Half-cell spectra as tool to determine location of RE-potential
- Cathode limitation is not neglectable





- Half-cell spectra as tool to determine location of RE-potential
- Cathode limitation is not neglectable
- RE potential is shifted away from the middle towards the anode





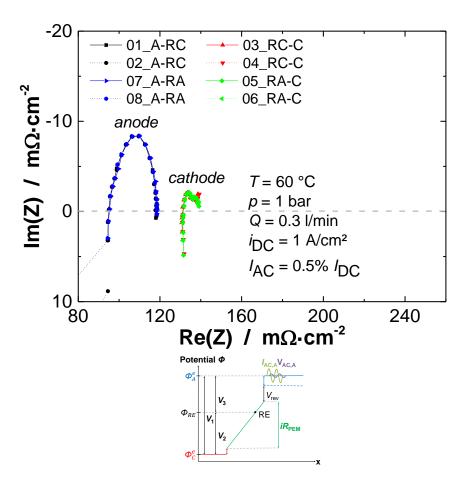


- Half-cell spectra as tool to determine location of RE-potential
- Cathode limitation is not neglectable
- RE potential is shifted away from the middle towards the anode
- Factor in calculation of overpotential which is not 1/2

$$f(?)$$

$$\downarrow$$

$$\eta_{\rm A} = V_3 - \frac{1}{2}i_{\rm cell} Z_1^* - V_{\rm rev}$$

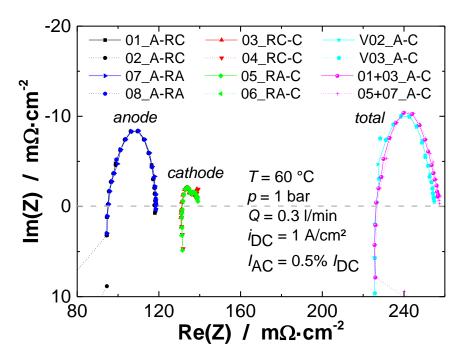




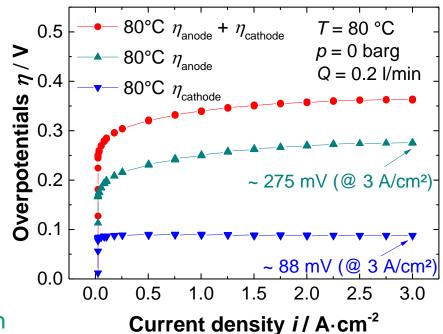


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f(?)
↓
η_A = V₃ -
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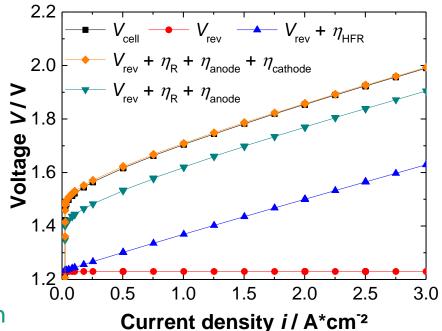


- Half-cell spectra as tool to determine location of RE-potential
- Separate examination of anodic and cathodic overvoltages
 - Separate degradation analysis
- E.g.: overpotentials @ 3 A/cm²
 - Anode ≈ 275 mV
 - Cathode ≈ 88 mV
 - → Separate anode and cathode in AST development



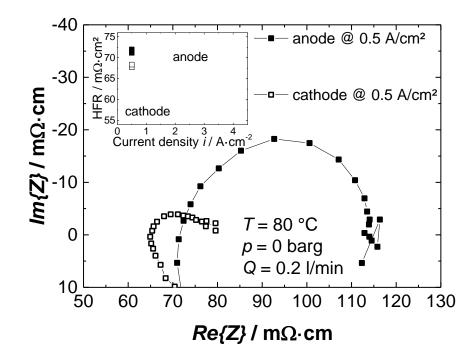


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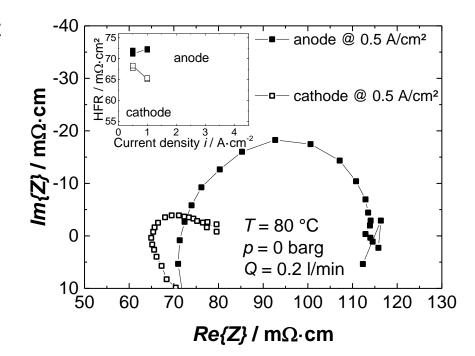


Half impedance spectra to extract HFR of anode and cathode



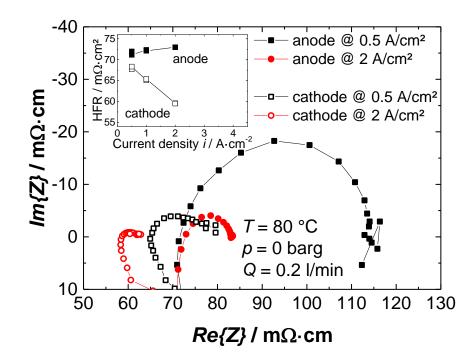


- Half impedance spectra to extract HFR of anode and cathode
- HFR is current dependant



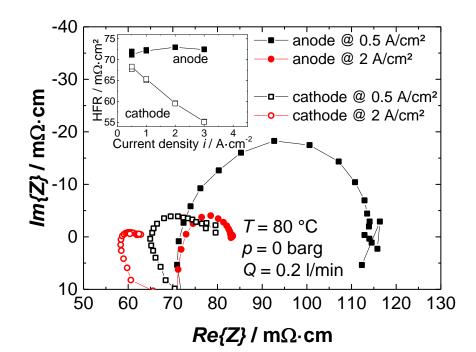


- Half impedance spectra to extract HFR of anode and cathode
- HFR is current dependant
- Cathode HFR decreases





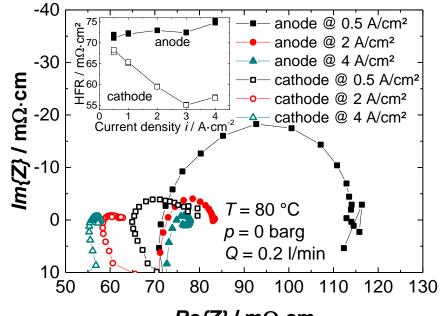
- Half impedance spectra to extract HFR of anode and cathode
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- Cathode HFR decreases





- Half impedance spectra to extract HFR of anode and cathode
- HFR is current dependant
- Cathode HFR decreases
- Anode HFR slightly increases
- Factor to calculate overvoltages is dependent on current

$$f_{\rm RE}(i) \\ \clubsuit \\ \eta_{\rm A} = V_3 - \frac{1}{2} i_{\rm cell} Z_1^* - V_{\rm rev}$$



Re{Z} / mΩ·cm

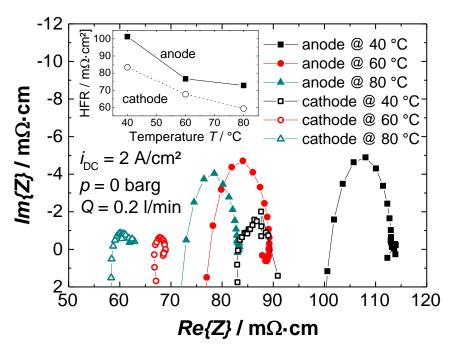


- Half impedance spectra to extract HFR of anode and cathode
- HFR is temperature dependant
- Cathode and anode HFR decreases
- Factor to calculate overvoltages is also dependent on temperature

$$f_{\rm RE}(i,T)$$

$$\downarrow$$

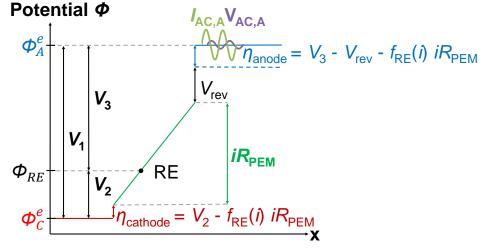
$$\eta_{\rm A} = V_3 - \frac{1}{2}i_{\rm cell} Z_1^* - V_{\rm rev}$$





- Reduction of HFR with increasing I and T coming mainly from cathodic side
 - Heat production on anodic side might influence PEM behavior
- Possible gradient in T inside the PEM individual HFR shifts?
- Possible gradient in water content (λ) inside the PEM?

```
\rightarrow AST development for PEM possible
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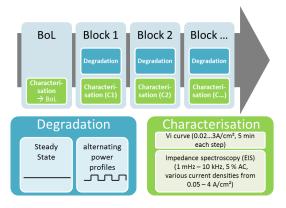
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Conclusion Summary

- Comprehensive understanding of in-situ characterization methods is necessary for AST development
 - RE-method for local separation of degradation effects
 - EIS for separation of transient behavior of degradation effects
 - Half-cell EIS for more insight and verification of both methods
- Evaluation of different operating profiles and their influence on degradation can be investigated more substantially
- Let's test different profiles





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 All members of the departments "Chemical Energy Storage" at Fraunhofer ISE

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Thank you for your attention!



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